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# Mobile flume for inverted semicircular Open channel 

 القناة الدحمولة للمجارى المفتو حة النصف دائرية المقلوبةHoda A. Matter, Mosaad Khadr and I.M.H. Rashwan



| ان قيّس العّبصرف خلا المجاري المانية المقتوحة جزء أساسي من إدارة المنظومة المانية ولقيكس قيم <br>  نقاط وتتم من خلال مرفة مسلاحة القطاع المائي حساب التصرف ـ وتوجد طرق الخرى تعتد علي تكوين قطاع <br>  <br>  <br> ويكن تصنيف المنشئت المستخذية لتكوين قطاع حرج لقياس التصرف إلي منثشآت ثابتة وأخري متتقلة. <br>  نصف دالنرى ولقت تم أختيار الجهاز بحيث يتم استخالم ماسورة رأسيةّ لخلق إنتّاق في القطاع لتّوليد سريان <br>  نظرية وأخري عطلية. الأراسة النظرية تم من خلالها دراسة شكل سريان المياه خلال الماسورة الأفقية <br>  معادلة رقم فرويد مما أدي إلي الوصول لمعالات مبسطة للربط بين الطاقة النوعية الحرجة وعمق المياه <br>  الطاقة الحرجة والعمق الّحرج مع التصرف في صورة لابعدية في جاولن وبيانيا ومن ثم استخذام الثنتائيج <br>  <br>  <br>  مباشرة وبنسبة خطا لاتتغى 8.7\%. |  |
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Abstract- The discharge measurement is significant in wide engineering applications such as water conveyance, sewer system, irrigation, and drainage system. Many devices are designed to measure discharge in partially filled circular and semicircular channels. In this study new semicircular mobile flume depends on the concept of developing a contracted zone to have a control section was examined. The contraction was made by installing a vertical pipe with axial holes at the semicircular open channel to create critical flow. To evaluate the efficiency of this type of devices mathematical and experimental studies were presented.

[^0]Specific energy, discharge, and Froude number equations were used to deduce the mathematical model. Experimental work was carried out in measuring the discharge values with known specific energy values. The experimental data was used to evaluate the mobile device to measure discharge. New equations for both discharge and discharge coefficient were presented. The verification leaded to have a discharge correction equation to calculate the discharge based on the contraction ratio and the measured water depth in the vertical pipe. Results of the comparison showed that the proposed model provided a reliable prediction of the discharge with high accuracy and maximum error up to $8.7 \%$.

## I INTRODUCTION

EASUREMENT of discharge in open channels

Mhas been a classical topic of interest to many engineers. When the water available from a particular source is limited and must be used very carefully, it is necessary to measure the discharge at various points in the system and the flow at
farmer's intakes. Some benefits of water measurement were listed by the U. S. Department of the Interior Bureau of Reclamation [1]. Simonovic [2], selected 27 methods for flow measurement from the handbook published by the International Organization for Standardization [3, 4].

### 1.1. Mobile Venturi Flume

There are two types of discharge measurement structure, either the structure is mounted permanently in the channel or the structure is temporarily positioned for discharge evaluation. The device may be mounted and removed quickly, and such device might then be referred to as a mobile device. Its major advantages include low cost, reading precision and rapid installation in running water. A Venturi body allows determining the discharge by a single depth reading. The mobile discharge measurement for rectangular, trapezoidal, triangular, U -shape and circular profiles is introduced.

### 1.2. Mobile Venturi Flume in Rectangular Channel

Balloffet [5] introduced simple elements for mobile discharge measurement in rectangular channels. Diskin [6] described a mobile arrangement for discharge measurement by using Venturi bodies similar to bridge piers instead of circular cylinders. In 1985, Hager [7] used a cylinder made of a high plastic material to make a contracted section to have with the critical flow in contracted rectangle channel. Hager [8] presented a modified Venturi type discharge measurement. Hager [9] declared that Ueberl and Hager (1994) tested the standard Venturi body in a rectangular channel. The Venturi body was provided with holes of about 5 mm diameter arranged along the front of the cylinder, with an inter distance of about 50 mm . If this line of holes is located against the flow direction, the flow depth in the cylinder equals to the stagnation head, i.e. the energy head H of the flow. Peruginelli and Bonacci [10] used mobile pier-shaped prism device to measure the discharge in a rectangular channel. Samani and Magallanez [11] attached a two semi cylinder of polyvinyl chloride (PVC) to the side wall of the rectangular channel. Wu and Molinas [12] developed a new discharge equation, which based on the conservation of energy and experimental data with a wide range of opening ratios. In 2004, threedimensional turbulent flow field at a vertical semicircular cylinder, attached to the sidewall of a rectangular channel, was taken in the laboratory using an Acoustic Doppler Velocimeter (ADV) [13]. Gole [14] estimated a discharge equation for free and submerged flow condition. Ghare and Badar [15], investigated experimentally and calibrated a simple mobile flume to measure a discharge through small rectangular open channels in agricultural fields.

### 1.3. Mobile Venturi with Circular Cone

Hager [16] used a circular cone to made contraction section through a rectangular channel.

### 1.4. Mobile Venturi in Trapezoidal Channel

In 1986, Hager [17] used a cylinder made of a high plastic material to make a contracted section with the critical flow in
the contracted trapezoidal channel. In 1993, Samani and Magallanez [18] used flume consisted of pipe installed axially inside a trapezoidal channel with side slope 1:1. In 2012, Badar and Ghare [19] developed a new mathematical model to predict the discharge through a trapezoidal canal by simple cylindrical flume using experimental data available in the literature for trapezoidal canal having 1:1 side slope.

### 1.5. Mobile Venturi in $U$-Shape Channel

Hager [9] explained the proposal of Hager and Züllig refers to a mobile flume inserted in a prefabricated U-shaped channel.

### 1.6. Mobile Venturi Flume in Circular Pipe

Hager [20] used a mobile device as shown in Fig. 1 to measure the discharge in partially field pipe. The device is a cylinder of diameter $\mathrm{d}<\mathrm{D}$ and the base of the cylinder is rounded to $\mathrm{D} / 2$. Using specific energy equation and Froude number led to having the following expressions:
$Q_{\text {me }} / Q_{\text {cal }}=0.985+0.205 E *$
Where $Q_{m e}$ is measured discharge, $Q_{c a l}$ is calculated discharge and $E *$ is the dimensionless specific energy $(E / D), D$ is the semicircular diameter.
Samani et al. [21] replaced the graphical approach presented by Hager, which was used to calibrate the water measuring device based on the measured value of upstream energy. The relation between the measured and the calculated discharge was as follows:
$Q_{\text {me }} / Q_{\text {cal }}=1.075+0.2266 E_{*}$


Fig. 1. Schematic plot of mobile device unit.
Kohler and Hager [22] improved the circular mobile flume to measure discharge in partially filled pipes, as the case in sewage and drainage engineering. Enciso [23], assessed the impact of the best management practices (BMPs) on water quality at selected agricultural fields located in the Arroyo Colorado watershed during two irrigation events in 2009 and 2010. He used a PVC mobile circular flume placed at the drainage ditch to measure runoff flow-rate using a data logger and a pressure transducer. Figure (2) shows schematic of the flume that was used to measure irrigation return flows. To assure that the circular flume measured accurately and with less than $10 \%$ error, the flow meter was calibrated in the Harlingen Irrigation District.


Fig. 2. Calibration of the circular flow meter in the Harlingen Irrigation District.
Rashwan and Idress [24] evaluated the efficiency of mobile flume as discharge measurement device for the partially filled circular channel. The experimental data was used to evaluate the mobile flume as a device to measure discharge. A general equation was developed for discharge coefficient $\left(C_{d}\right)$ as:
$C_{d}=((7.3839) \delta-1.9348)+((4.4912) \delta-0.2883) E_{*_{\text {me }}}$
Where $C_{d}$ is discharged coefficient, $E_{*_{m e}}$ is the dimensionless specific energy $\left(E_{m e} / D\right)$ and $\delta$ is contraction ratio $(d / D)$.

In 2016, Davis and Samani [25] produced manually for simple flow measurement devices in open channels. This manual is divided into two main chapters; the first one outlines the design characteristics of simple flow measurement devices which are typically easier and less expensive to be produced. The second chapter investigates more traditional flow measurement devices and illustrates the strengths and weaknesses of both types. In 2017, Zohrab Samani [26] discussed the design and the calibration of three simple flumes for flow measurements in open channels. The flumes were designed based on principles of critical flow in open channels. The critical flow was created through the contraction of the flow cross section by installing vertical cylindrical columns in an open channel.

In the present study, a semicircular mobile flume is proposed to measure discharge in the small open channel. This mobile device consists of a vertical pipe with diameter $d$ fixed on semicircular flume with diameter $D$. The presence of the vertical pipe reduces the cross section of the flow and creates a critical flow condition.

## II Mathematical Work

There are several types of flow measurement devices currently in use across the world. The most common flume designs, in use nowadays, include the Parshall flume, the Cutthroat flume, the Trapezoidal flume, and the Mobile flume. The mobile flume with rectangular, triangular, trapezoidal, Ushape and circular cross-sections was developed earlier. The present study provides a new arrangement mobile with an inverted semicircular section that can be used as a measurement device in a partially filled pipe.

The discharge equation is estimated by using specific energy equation, discharge equation, and Froude number equation. The assumptions to estimate the discharge equation led to having an error in the calculated discharge value. This error has to be corrected; therefore an expression of the
correction factor was driven to have the actual value of the discharge.

### 2.1. Governing Equations

Chow [27] reported that Bakhmeteff (1912) introduced the specific energy term as the energy of water at any section of the channel with respect to the channel bottom as a datum as follows,

$$
\begin{equation*}
E=d_{w} \cos \theta+\frac{\alpha V^{2}}{2 g} \tag{4}
\end{equation*}
$$

Where $E$ is the specific energy, $d_{w}$ is the normal depth of the point below the water surface, $\theta$ is the slope angle of the channel bottom, $\alpha$ is the energy coefficient due to variable velocity distribution, $V$ is the stream line velocity and $g$ is the gravitational acceleration.

For a channel of small slope (mild) or horizontal, the section depth is more or less the same as the water depth $\left(d_{w} \cos \theta \approx y\right)$. The ideal parallel flow has a uniform velocity distribution. This type of flow has unity energy coefficient ( $\alpha$ $\approx 1$ ). Therefore, for ideal parallel flow, the energy head can be written with substitute the term of the velocity in Eq. (4) by discharge term $(Q / A)$ as follows:

$$
\begin{equation*}
E=y+\frac{Q^{2}}{2 g A^{2}} \tag{5}
\end{equation*}
$$

Where $y$ is the water depth, $Q$ is the discharge and $A$ is an area of the water section.
For a semicircular channel with diameter $D$, divided Eq. (5) by $D$ yields to

$$
\begin{equation*}
E_{*}=Y+\frac{Q_{*}^{2}}{2 A_{*}^{2}} \tag{6}
\end{equation*}
$$

Where $Y$ is the relative water depth $(y / D), Q_{*}$ is the dimensionless discharge $\left(\sqrt{Q^{2} / g D^{5}}\right)$ and $A_{*}$ is dimensionless water area $\left(A / D^{2}\right)$.

### 2.2. Inverted Semicircular Mobile Device

The main contracted section on the semicircular mobile flume is controlled section. This section is shown in Figure (3).


Fig. 3. Contracted sections through semicircular mobile flume
The discharge, through semicircular mobile flume, can be estimated by using specific energy, discharge, and Froude number equations.

The contracted section is contracted by a vertical cylinder with outside diameter $(d)$ which made contraction ratio $\delta(d / D)$ as shown in Figure (4).


Fig. 4. Geometric properties of contracted section

The geometric properties of the contracted inverted semicircular section can be easily computed as follows

$$
\begin{equation*}
A_{*}=\frac{\phi-\sin \phi-\pi}{8}-\delta(Y) \tag{7}
\end{equation*}
$$

Where $\phi$ is the central angle and $\delta$ is the relative diameter of the vertical cylinder ( $d / D$ )
The top width at contracted section can be calculated as, Fig. (4);

$$
\begin{equation*}
\frac{T}{2}+\frac{d}{2}=\sqrt{\left(\frac{D}{2}\right)^{2}-(y)^{2}} \tag{8}
\end{equation*}
$$

Where $T$ is top width at the contracted section.
Divided Eq. (8) by $D$ yields to

$$
\begin{equation*}
T_{*}=2 \sqrt{0.25-(Y)^{2}}-\delta \tag{9}
\end{equation*}
$$

Where $T_{*}$ is dimensionless top width at contracted section
According to the water profile through the flume pipe, the critical flow happened at the contraction section. So, at the contraction zone, the relative specific energy can be written as

$$
\begin{equation*}
E_{*_{c}}=Y_{c}+\frac{A_{*_{c}}}{2 T_{*_{c}}} \tag{10}
\end{equation*}
$$

Where $E_{*_{c}}$ is the relative critical specific energy, $Y_{c}$ is the relative critical water depth $\left(y_{c} / D\right), A_{*_{c}}$ is the relative critical water area and $T_{*_{C}}$ is the relative critical water top width.

The above equation used to find relative critical water depth $\quad\left(Y_{c}\right)$, from knowing dimensionless critical specific energy $\quad\left(E_{*_{c}}\right)$. By putting Eq. (7) and Eq. (9) in Eq. (10) one obtains:

$$
\begin{equation*}
E_{*}=Y_{c}+\frac{\phi-\sin \phi-\pi-8 \delta\left(Y_{c}\right)}{16\left(2 \sqrt{0.25-\left(Y_{c}\right)^{2}}-\delta\right)} \tag{11}
\end{equation*}
$$

The general equation of Froude number is as follows;
$F_{r}^{2}=\frac{Q^{2} T}{g A^{3}}=\frac{Q^{2}(T / D)}{g D^{5}\left(A / D^{2}\right)^{3}}=\frac{Q_{*}^{2} T_{*}}{A_{*}{ }^{3}}$
Where $F_{r}^{2}$ is Froude number
Applying equation (12) for critical flow, $F_{r}^{2}=1.0$ and $y=y_{c}$ yields the following expression:

$$
\begin{equation*}
Q *{ }^{2}=\frac{A_{* c}{ }^{3}}{T_{* c}} \tag{13}
\end{equation*}
$$

Substituting Eq. (7) and (9) in Eq. (12) gives:

$$
\begin{equation*}
Q_{*}=\left[\frac{\left(\phi-\sin \phi-\pi-8 \delta\left(Y_{c}\right)\right)^{3}}{512\left(2 \sqrt{0.25-\left(Y_{c}\right)^{2}}-\delta\right)}\right]^{1 / 2} \tag{14}
\end{equation*}
$$

### 2.2. Proposed Model

The main problem of the study is the determination of the discharge value, and this can be done using the proposed model with the following steps:

1. Measure the water depth through the contraction device which can be regarded as critical specific energy $\left(E_{m e}\right)$;
2. Divide the critical specific energy by the diameter $(D)$ to get the relative critical specific energy $\left(E_{*_{c}}\right)$;
3. Estimate the value of relative critical water depth $\left(Y_{c}\right)$ by knowing the value of the relative critical specific energy and $\delta$ from Eq. (11). The solution of this equation can be done by trial and error, or by using tables, or from the graph.
4. Using the relative critical water depth, the required discharge can be calculated from Eq. (14).

## III EXPERIMENTAL WORK

Diagrammatic sketch for the experimental flume is shown in Fig (5).


1- Ground water tank
2- 10 H.P pump
3- Control valve
4- Inlet channel
5- Upstream sluice gate
6- Vertical cylinder

7- Plastic semicircular pipe
8- Downstream gate
9- End channel part
10- Inner collected tank
11- Rectangular notch
12- Return pipe

Fig. 5. Diagrammatic sketch for the Flume.
A storage tank of $12.00 \mathrm{~m}^{3}$ was made to feed the flume by water requirement. The flow of water through supplier pipe and flume can
be obtained by 10 H.P pump. A valve at the downstream side of the pump was used to control discharge value. Precaution from turbulence at the inlet of flume was used in the first part of the flume to have uniform flow. The flume dimensions are 14.25 m long, 1.00 m wide and 1.00 m height. It was divided into three sections. The first one was used to remove eddies and to give a uniform flow condition. The second part of flume has a Plexiglas plate as a side to have a clear view during the experimental work. The development of models based on the design of simple flume for flow measurement in the open channel was proposed. The semicircular contraction flume was constructed by placing a vertical circular cylinder inside the semicircular pipe portion of the hydraulic flume. In the present experiment, semicircular pipe with three different diameters and three different contractions were prepared, (Table 1).

TABLE 1
Contracted ratios and pipe diameters

| Pipe Diameter D <br> $(\mathbf{c m})$ |  | Contraction Ratios |  |  |
| :--- | :--- | :--- | :--- | :--- |
|  | 32.4 \% | 41.3 \% | 47.5 \% |  |
| internal | external | Vertical Pipe Diameter d |  |  |
| 15.00 | 16.00 | 4.86 | 5.90 | 7.84 |
| 18.40 | 20.00 | 6.20 | 7.60 | 16.70 |
| 24.20 | 26.20 | 7.13 | 8.70 | 11.50 |

TABLE 2
EXPERIMENTAL RESULTS

| $\begin{aligned} & \text { Run } \\ & \text { No. } \end{aligned}$ | $\begin{aligned} & Q_{m e} \\ & (\mathrm{~cm} 3 / \mathrm{s}) \end{aligned}$ | $\delta=0.324$ |  | $\delta=0.413$ |  | $\delta=0.475$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | $\begin{array}{r} E_{m e} \\ (\mathrm{~cm}) \\ \hline \end{array}$ | $E_{*_{m e}}$ | $\begin{gathered} E_{\text {me }} \\ (\mathrm{cm}) \\ \hline \end{gathered}$ | $E_{*_{\text {me }}}$ | $\begin{array}{r} E_{\text {me }} \\ (\mathrm{cm}) \\ \hline \end{array}$ | $E_{*}{ }_{\text {me }}$ |
| 1 | 685 | 2.5 | 0.1033 | 2.6 | 0.1074 | 2.7 | 0.1116 |
| 2 | 921 | 2.9 | 0.1198 | 3.0 | 0.1240 | 3.2 | 0.1322 |
| 3 | 1501 | 3.6 | 0.1488 | 3.7 | 0.1529 | 4.1 | 0.1694 |
| 4 | 1611 | 3.8 | 0.1570 | 4.0 | 0.1653 | 4.2 | 0.1736 |
| 5 | 1932 | 4.2 | 0.1736 | 4.3 | 0.1777 | 4.5 | 0.1860 |
| 6 | 2281 | 4.5 | 0.1860 | 4.6 | 0.1901 | 4.8 | 0.1983 |
| 7 | 2440 | 4.6 | 0.1901 | 4.8 | 0.1983 | 5.0 | 0.2066 |
| 8 | 2531 | 4.8 | 0.1983 | 4.9 | 0.2025 | 5.1 | 0.2107 |
| 9 | 2730 | 4.9 | 0.2025 | 5.0 | 0.2066 | 5.2 | 0.2149 |
| 10 | 2813 | 5.0 | 0.2066 | 5.2 | 0.2149 | 5.4 | 0.2231 |
| 11 | 2933 | 5.1 | 0.2107 | 5.3 | 0.2190 | 5.5 | 0.2273 |
| 12 | 3054 | 5.2 | 0.2149 | 5.4 | 0.2231 | 5.6 | 0.2314 |
| 13 | 3326 | 5.3 | 0.2190 | 5.6 | 0.2314 | 5.8 | 0.2397 |
| 14 | 3452 | 5.4 | 0.2231 | 5.7 | 0.2355 | 5.9 | 0.2438 |
| 15 | 3529 | 5.4 | 0.2231 | 5.7 | 0.2355 | 6.2 | 0.2562 |
| 16 | 3606 | 5.4 | 0.2231 | 5.8 | 0.2397 | 6.3 | 0.2603 |
| 17 | 3813 | 5.6 | 0.2314 | 5.8 | 0.2397 | 6.0 | 0.2479 |
| 18 | 4023 | 5.7 | 0.2355 | 6.2 | 0.2562 | 6.4 | 0.2645 |
| 19 | 4103 | 5.9 | 0.2438 | 6.1 | 0.2521 | 6.3 | 0.2603 |
| 20 | 4278 | 5.9 | 0.2438 | 6.5 | 0.2686 | 6.7 | 0.2769 |
| 21 | 4482 | 6.1 | 0.2521 | 6.3 | 0.2603 | 6.5 | 0.2686 |
| 22 | 4675 | 6.5 | 0.2686 | 6.7 | 0.2769 | 6.9 | 0.2851 |
| 23 | 4885 | 6.3 | 0.2603 | 6.7 | 0.2769 | 7.2 | 0.2975 |
| 24 | 5370 | 6.6 | 0.2727 | 7.0 | 0.2893 | 7.5 | 0.3099 |
| 25 | 5721 | 7.0 | 0.2893 | 7.2 | 0.2975 | 7.4 | 0.3058 |
| 26 | 6094 | 7.2 | 0.2975 | 7.4 | 0.3058 | 7.6 | 0.3140 |
| 27 | 6214 | 7.3 | 0.3017 | 7.7 | 0.3182 | 7.9 | 0.3264 |
| 28 | 7173 | 8.0 | 0.3306 | 8.3 | 0.3430 | 8.5 | 0.3512 |
| 29 | 7652 | 8.1 | 0.3347 | 8.4 | 0.3471 | 8.6 | 0.3554 |
| 30 | 8042 | 8.2 | 0.3388 | 8.5 | 0.3512 | 8.7 | 0.3595 |

The water depth in the semicircular pipe can be read using piezometer. Discharge through the experimental flume was determined using a rectangular notch at the flume sump. Once the
cylinder was fixed in the circular channel, discharge was varied from $Q \min =0.685 \mathrm{~L} / \mathrm{s}$ to $\max =8.042 \mathrm{~L} / \mathrm{s}$. For each discharge, the approaching depth of flow in the semicircular pipe channel was observed and the energy head was evaluated. Then this quantity was equal to critical energy head, the sought relation $Q_{m e} / E_{m e}$ can be established (Table 2).


Plate (1) Second part of Flume

## IV ANALYSIS AND DISCUSSIONS

The main objective of the present study is to get the discharge using the mobile flume in the semicircular open channel for values of contraction ratio $\delta$. With $E_{*_{c}}$ and $Y c$ that is presented in Eq. (11). The corresponding dimensionless discharge $Q_{*}$ can be computed from Eq. (12). Table 3 shows the values of $E_{*_{c}}$ and $Q_{*}$ corresponding to values of $Y c$ for contraction ratios $\delta=0.324,0.413$ and 0.475 .

TABLE 3
Values of critical specific energy $E_{*_{c}} Q_{\text {and }} Q_{\text {Corresponding to }}$

| $Y_{c}$ | $\delta=0.324$ |  | $\delta=0.413$ |  | $\delta=0.475$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $Q_{*}$ | $E_{* c}$ | $Q_{*}$ | $E_{*}$ | $Q_{*}$ | $E_{*}{ }_{c}$ |
| 0.000 | 0.00000 | 0.00000 | 0.00000 | 0.00000 | 0.00000 | 0.00000 |
| 0.020 | 0.00188 | 0.02989 | 0.00163 | 0.02987 | 0.00145 | 0.02986 |
| 0.040 | 0.00536 | 0.05995 | 0.00465 | 0.05994 | 0.00415 | 0.05993 |
| 0.060 | 0.00988 | 0.09010 | 0.00857 | 0.09011 | 0.00766 | 0.09013 |
| 0.080 | 0.01523 | 0.12040 | 0.01322 | 0.12046 | 0.01181 | 0.12052 |
| 0.100 | 0.02131 | 0.15091 | 0.01849 | 0.15105 | 0.01653 | 0.15118 |
| 0.120 | 0.02803 | 0.18169 | 0.02433 | 0.18196 | 0.02176 | 0.18221 |
| 0.140 | 0.03535 | 0.21282 | 0.03069 | 0.21328 | 0.02745 | 0.21370 |
| 0.160 | 0.04323 | 0.24440 | 0.03754 | 0.24513 | 0.03358 | 0.24580 |
| 0.180 | 0.05165 | 0.27652 | 0.04487 | 0.27764 | 0.04015 | 0.27867 |
| 0.200 | 0.06059 | 0.30934 | 0.05266 | 0.31099 | 0.04714 | 0.31254 |
| 0.220 | 0.07006 | 0.34303 | 0.06093 | 0.34542 | 0.05459 | 0.34769 |
| 0.240 | 0.08008 | 0.37783 | 0.06971 | 0.38125 | 0.06252 | 0.38453 |
| 0.260 | 0.09068 | 0.41406 | 0.07905 | 0.41892 | 0.07099 | 0.42364 |
| 0.280 | 0.10193 | 0.45216 | 0.08904 | 0.45905 | 0.08014 | 0.46590 |
| 0.300 | 0.11395 | 0.49277 | 0.09982 | 0.50261 | 0.09014 | 0.51264 |
| 0.320 | 0.12692 | 0.53685 | 0.11166 | 0.55109 | 0.10131 | 0.56611 |
| 0.340 | 0.14115 | 0.58592 | 0.12497 | 0.60702 | 0.11425 | 0.63032 |
| 0.360 | 0.15716 | 0.64254 | 0.14052 | 0.67503 | 0.13004 | 0.71326 |
| 0.380 | 0.17589 | 0.71142 | 0.15980 | 0.76455 | 0.15110 | 0.83350 |
| 0.400 | 0.19919 | 0.80229 | 0.18620 | 0.89857 | 0.18385 | 1.04666 |
| 0.420 | 0.23137 | 0.93930 | 0.22942 | 1.15174 | 0.25455 | 1.63035 |
| 0.440 | 0.28526 | 1.20418 | 0.33684 | 1.98567 | ------ | ------ |
| 0.460 | 0.43146 | 2.17502 | ------ | ------ | ------ | ------ |

Figure (6) shows the plot for the critical depth Yc with critical specific energy $E_{* c}$ for contraction ratios $\delta=0.324,0.413$ and 0.475 .


Fig. 6. Critical depth $Y c$ with critical specific energy $E_{*_{C}}$ for contraction ratios $\delta=0.324,0.413$ and 0.475 .

A relative critical water depth plot as ordinate against the dimensionless measured specific energy as abscissa will appear approximately as a straight line for specific energy less than 0.5 regardless of the device diameter. The final result corresponds to explicit equations for critical water depth once the specific energy height in the vertical pipe at contraction section is recorded.
Also, Figure (7) shows the plot for the Discharge $Q_{*}$ with critical specific energy $E_{* c}$ for the same contraction ratios.


Fig. 7. Discharge $Q_{*}$ versus critical specific energy $E_{* c}$ for contraction ratios

$$
\delta=0.324,0.413 \text { and } 0.475
$$

According to experimental work (Table (1)), the relationship between measured discharge and measured specific energy can be easily plotted. Figure (8) shows the dimensionless measured discharge $Q_{* m e}$ with dimensionless measured critical specific energy $E_{* m e}$ for contraction ratios $\delta$ $=0.324,0.413$ and 0.475 .


Fig. 8. Discharge $Q_{* m e}$ versus measured critical specific energy $E_{* m e}$ for contraction ratios $\delta=0.324,0.413$ and 0.475 .

Using the least-squares techniques, the relationship between the dimensionless measured discharge, $Q_{*_{m e}}$ and the dimensionless measured specific energy $\quad E_{*_{m e}}$ can be written as follows:

$$
\begin{array}{lll}
Q_{*}=0.8409 E_{* m e}^{2.0721} & \delta=0.324 & R^{2}=0.9964 \\
Q_{*}=0.7454 E_{* m e}^{2.0502} & \delta=0.413 & R^{2}=0.9975 \\
Q_{*}=0.7362 E_{* m e}^{2.1035} & \delta=0.475 & R^{2}=0.995 \tag{17}
\end{array}
$$

The percentage error for the calculated discharge is:

$$
\begin{equation*}
\text { Error }=\frac{Q_{m e}-Q_{c a l}}{Q_{m e}} \times 100 \tag{18}
\end{equation*}
$$

The error percentages in calculating the dimensionless discharge value for various contraction ratios are tabulated in Table (4).

However, the estimated discharge according to Eqs. (15), (16) and (17) deviates from the measured one. The calculated flow rates were compared with the measured rates. The comparison is presented in Table 3. Table 3 shows that the calculated discharge deviates the measured discharge by $6.7 \%$, $6.2 \%$ and $8.6 \%$ for contraction ratios $\delta=0.324,0.413$ and 0.475 respectively.

The error percentages in the calculated dimensionless discharge values for various contraction ratios are tabulated in Table (5).

TABLE 4 COMPARISON OF MEASURED AND CALCULATED DISCHARGE FOR VARIOUS CONTRACTION RATIO ( $\Delta$ )

|  | $\begin{aligned} & Q_{m e} \\ & (\mathrm{~cm} 3 / \\ & \mathrm{s}) \end{aligned}$ | $\delta=0.324$ |  | $\delta=0.413$ |  | $\delta=0.475$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\underset{\sim}{\square} \dot{Z}$ |  | $\begin{aligned} & Q_{c a l} \\ & (\mathrm{~cm} 3 / \mathrm{s}) \\ & \text { Eq. }(15) \end{aligned}$ | $\begin{aligned} & \text { Error } \\ & \% \end{aligned}$ | $Q_{\text {cal }}$ <br> (cm3/s) <br> Eq. <br> (16) | $\begin{aligned} & \text { Error } \\ & \% \end{aligned}$ | $Q_{c a l}$ <br> (cm3/s) <br> Eq. <br> (17) | 䓪 |
| 1 | 685 | 688 | -0.4 | 694 | -1.3 | 659 | 3.8 |
| 2 | 921 | 935 | -1.5 | 931 | -1.0 | 942 | -2.2 |
| 3 | 1501 | 1464 | 2.5 | 1431 | 4.7 | 1587 | -5.7 |
| 4 | 1611 | 1637 | -1.6 | 1679 | -4.2 | 1669 | -3.6 |
| 5 | 1932 | 2014 | -4.3 | 1947 | -0.8 | 1930 | 0.1 |
| 6 | 2281 | 2324 | -1.9 | 2236 | 2.0 | 2211 | 3.1 |
| 7 | 2440 | 2432 | 0.3 | 2440 | 0.0 | 2409 | 1.3 |
| 8 | 2531 | 2657 | -4.9 | 2545 | -0.5 | 2511 | 0.8 |
| 9 | 2730 | 2772 | -1.6 | 2653 | 2.8 | 2616 | 4.2 |
| 10 | 2813 | 2891 | -2.8 | 2875 | -2.2 | 2832 | -0.7 |
| 11 | 2933 | 3012 | -2.7 | 2989 | -1.9 | 2944 | -0.4 |
| 12 | 3054 | 3136 | -2.7 | 3106 | -1.7 | 3057 | -0.1 |
| 13 | 3326 | 3262 | 1.9 | 3347 | -0.6 | 3291 | 1.1 |
| 14 | 3452 | 3391 | 1.8 | 3470 | -0.5 | 3412 | 1.2 |
| 15 | 3529 | 3391 | 3.9 | 3470 | 1.7 | 3787 | -7.3 |
| 16 | 3606 | 3391 | 6.0 | 3596 | 0.3 | 3917 | -8.6 |
| 17 | 3813 | 3656 | 4.1 | 3596 | 5.7 | 3535 | 7.3 |
| 18 | 4023 | 3793 | 5.7 | 4123 | -2.5 | 4049 | -0.6 |
| 19 | 4103 | 4074 | 0.7 | 3988 | 2.8 | 3917 | 4.5 |
| 20 | 4278 | 4074 | 4.8 | 4543 | -6.2 | 4458 | -4.2 |
| 21 | 4482 | 4365 | 2.6 | 4261 | 4.9 | 4183 | 6.7 |
| 22 | 4675 | 4979 | -6.5 | 4834 | -3.4 | 4743 | -1.4 |
| 23 | 4885 | 4667 | 4.5 | 4834 | 1.0 | 5187 | -6.2 |
| 24 | 5370 | 5139 | 4.3 | 5288 | 1.5 | 5652 | -5.2 |
| 25 | 5721 | 5806 | -1.5 | 5602 | 2.1 | 5495 | 4.0 |
| 26 | 6094 | 6154 | -1.0 | 5926 | 2.8 | 5812 | 4.6 |
| 27 | 6214 | 6333 | -1.9 | 6429 | -3.5 | 6305 | -1.5 |
| 28 | 7173 | 7656 | -6.7 | 7498 | -4.5 | 7354 | -2.5 |
| 29 | 7652 | 7856 | -2.7 | 7685 | -0.4 | 7538 | 1.5 |
| 30 | 8042 | 8058 | -0.2 | 7873 | 2.1 | 7723 | 4.0 |

However, the calculated discharge according to Eq. (14) deviates from the measured one. The calculated flow rates were compared with those measured. The comparison is presented in Table 4. Table 4 shows that the calculated discharge deviates the measured one by $59.4 \%, 47.6 \%$ and $56.1 \%$ for contraction ratios $\delta=0.324,0.413$ and 0.475 respectively. Therefore, the estimated equation must be corrected by the discharge coefficient.

### 4.1 Discharge Coefficient Equation

The relationship between the discharge coefficients $\left(C_{d}=Q_{* m e} / Q_{* c a}\right)$ versus dimensionless measured specific energy for various contraction ratios are shown in Fig (9).
Equations were developed for the discharge coefficient (Cd) based on the data in Fig. (9), using the least-squares techniques as follows:

$$
\begin{equation*}
Q_{m e} / Q_{c a}=2.9946 E_{* m e}+0.3276 \quad \delta=0.324 \quad R^{2}=0.9435 \tag{19}
\end{equation*}
$$

$$
\begin{equation*}
Q_{m e} / Q_{c a}=2.8248 E_{* m e}+0.4151 \quad \delta=0.413 \quad R^{2}=0.9628 \tag{20}
\end{equation*}
$$

$$
\begin{equation*}
Q_{m e} / Q_{c a}=3.2055 E_{* m e}+0.3554 \quad \delta=0.475 \quad R^{2}=0.943 \tag{21}
\end{equation*}
$$



Applying discharge coefficient equation led to decrease the percentage of error between the corrected calculated dimensionless discharges and measured one for contraction ratios, Table (4).

TABLE 5
COMPARISON OF MEASURED AND CALCULATED DISCHARGE USING EQ．（11）AND EQ．（14）FOR VARIOUS CONTRACTION RATIO（ $\Delta$ ）．

| 彦 | $\begin{aligned} & Q_{m e} \\ & \mathrm{cm3} / \mathrm{s} \end{aligned}$ | $\delta=0.324$ |  |  | $\delta=0.413$ |  |  | $\delta=0.475$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | $C_{d}$ | $Q_{\text {cal }} \mathrm{cm3/s}$ | 怱碞 | $C_{d}$ | $Q_{\text {cal }}$ cm3／s | 怱碞 | $C_{d}$ | $Q_{\text {cal }} \mathrm{cm3/s}$ | 気㤩 |
| 1 | 685 | 0.627 | 1092 | －59．4 | 0.678 | 1011 | －47．6 | 0.723 | 947 | －27．7 |
| 2 | 921 | 0.676 | 1363 | －47．9 | 0.740 | 1245 | －35．1 | 0.756 | 1218 | －24．4 |
| 3 | 1501 | 0.800 | 1877 | －25．0 | 0.885 | 1696 | －13．0 | 0.853 | 1760 | －14．7 |
| 4 | 1611 | 0.790 | 2039 | －26．6 | 0.846 | 1904 | －18．2 | 0.879 | 1832 | －12．1 |
| 5 | 1932 | 0.817 | 2364 | －22．4 | 0.911 | 2121 | －9．8 | 0.956 | 2021 | －4．4 |
| 6 | 2281 | 0.872 | 2617 | －14．7 | 0.976 | 2337 | －2．4 | 1.028 | 2220 | 2.8 |
| 7 | 2440 | 0.901 | 2707 | －11．0 | 0.980 | 2490 | －2．1 | 1.036 | 2355 | 3.6 |
| 8 | 2531 | 0.879 | 2878 | －13．7 | 0.988 | 2563 | －1．2 | 1.044 | 2424 | 4.4 |
| 9 | 2730 | 0.920 | 2969 | －8．7 | 1.033 | 2644 | 3.2 | 1.096 | 2490 | 9.6 |
| 10 | 2813 | 0.922 | 3050 | －8．4 | 1.006 | 2797 | 0.6 | 1.066 | 2638 | 6.6 |
| 11 | 2933 | 0.934 | 3140 | －7．1 | 1.019 | 2878 | 1.9 | 1.083 | 2707 | 8.3 |
| 12 | 3054 | 0.945 | 3230 | －5．8 | 1.032 | 2960 | 3.1 | 1.099 | 2779 | 9.9 |
| 13 | 3326 | 0.999 | 3330 | －0．1 | 1.065 | 3122 | 6.1 | 1.138 | 2924 | 13.8 |
| 14 | 3452 | 1.010 | 3420 | 0.9 | 1.080 | 3198 | 7.4 | 1.152 | 2996 | 15.2 |
| 15 | 3529 | 1.032 | 3420 | 3.1 | 1.103 | 3198 | 9.4 | 1.095 | 3221 | 9.5 |
| 16 | 3606 | 1.054 | 3420 | 5.1 | 1.101 | 3276 | 9.2 | 1.095 | 3294 | 9.5 |
| 17 | 3813 | 1.056 | 3609 | 5.3 | 1.164 | 3276 | 14.1 | 1.243 | 3068 | 24.3 |
| 18 | 4023 | 1.088 | 3700 | 8.0 | 1.112 | 3618 | 10.1 | 1.195 | 3366 | 19.5 |
| 19 | 4103 | 1.058 | 3880 | 5.4 | 1.160 | 3537 | 13.8 | 1.246 | 3294 | 24.6 |
| 20 | 4278 | 1.103 | 3880 | 9.3 | 1.108 | 3862 | 9.7 | 1.191 | 3591 | 19.1 |
| 21 | 4482 | 1.099 | 4079 | 9.0 | 1.212 | 3700 | 17.5 | 1.303 | 3441 | 30.3 |
| 22 | 4675 | 1.047 | 4467 | 4.5 | 1.159 | 4033 | 13.7 | 1.248 | 3746 | 24.8 |
| 23 | 4885 | 1.142 | 4277 | 12.4 | 1.211 | 4033 | 17.4 | 1.230 | 3970 | 23.0 |
| 24 | 5370 | 1.176 | 4566 | 15.0 | 1.253 | 4286 | 20.2 | 1.277 | 4205 | 27.7 |
| 25 | 5721 | 1.149 | 4981 | 12.9 | 1.281 | 4466 | 21.9 | 1.387 | 4125 | 38.7 |
| 26 | 6094 | 1.177 | 5179 | 15.0 | 1.311 | 4647 | 23.7 | 1.425 | 4277 | 42.5 |
| 27 | 6214 | 1.177 | 5279 | 15.1 | 1.266 | 4909 | 21.0 | 1.375 | 4518 | 37.5 |
| 28 | 7173 | 1.195 | 6001 | 16.3 | 1.318 | 5441 | 24.1 | 1.436 | 4995 | 43.6 |
| 29 | 7652 | 1.254 | 6100 | 20.3 | 1.381 | 5540 | 27.6 | 1.511 | 5065 | 51.1 |
| 30 | 8042 | 1.295 | 6208 | 22.8 | 1.430 | 5622 | 30.1 | 1.561 | 5152 | 56.1 |

From Table（4）it can be clearly seen that Eq．（14）has an error percentage of 0.3 up to $7.0 \%, 0.1$ up to $6.2 \%$ and 0 up to $8.7 \%$ for contraction ratios $32.4,41.3$ and $47.5 \%$ respectively．

Also，it can be noticed that the best contraction ratio used in the semicircular mobile flume is 0.413 ，which gives the discharge coefficient less than other contractions．

TABLE 6
COMPARISON OF CORRECTED CALCULATED AND MEASURED DISCHARGE.

| Run No. | $Q_{m e}{ }_{\text {cm } 3 / \mathrm{s}}$ | $\delta=0.324$ |  |  | $\delta=0.413$ |  |  | $\delta=0.475$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | $C_{d}$ | $Q_{\text {cal }}{ }_{\text {cm3/s }}$ | $\underset{\%}{\text { Error }} \begin{gathered} \end{gathered}$ | $C_{d}$ | $Q_{\text {cal }}{ }_{\text {cm3/s }}$ | $\begin{gathered} \text { Error } \\ \% \end{gathered}$ | $C_{d}$ | $Q_{c a l}{ }_{\text {cm3/s }}$ | $\begin{gathered} \text { Error } \\ \% \end{gathered}$ |
| 1 | 685 | 0.637 | 724 | -5.8 | 0.719 | 726 | -6.0 | 0.713 | 676 | 1.4 |
| 2 | 921 | 0.686 | 965 | -4.8 | 0.765 | 953 | -3.4 | 0.779 | 949 | -3.0 |
| 3 | 1501 | 0.773 | 1476 | 1.7 | 0.847 | 1437 | 4.3 | 0.898 | 1581 | -5.3 |
| 4 | 1611 | 0.798 | 1650 | -2.4 | 0.882 | 1679 | -4.2 | 0.912 | 1670 | -3.7 |
| 5 | 1932 | 0.847 | 2018 | -4.5 | 0.917 | 1945 | -0.6 | 0.951 | 1923 | 0.5 |
| 6 | 2281 | 0.884 | 2322 | -1.8 | 0.952 | 2225 | 2.5 | 0.991 | 2200 | 3.6 |
| 7 | 2440 | 0.897 | 2432 | 0.3 | 0.975 | 2429 | 0.4 | 1.018 | 2397 | 1.8 |
| 8 | 2531 | 0.922 | 2650 | -4.7 | 0.987 | 2530 | 0.1 | 1.031 | 2499 | 1.3 |
| 9 | 2730 | 0.934 | 2767 | -1.4 | 0.999 | 2641 | 3.3 | 1.044 | 2601 | 4.7 |
| 10 | 2813 | 0.946 | 2876 | -2.3 | 1.022 | 2859 | -1.6 | 1.071 | 2825 | -0.4 |
| 11 | 2933 | 0.959 | 2997 | -2.2 | 1.034 | 2976 | -1.5 | 1.084 | 2934 | 0.0 |
| 12 | 3054 | 0.971 | 3119 | -2.1 | 1.045 | 3094 | -1.3 | 1.097 | 3049 | 0.2 |
| 13 | 3326 | 0.983 | 3252 | 2.2 | 1.069 | 3337 | -0.3 | 1.124 | 3285 | 1.2 |
| 14 | 3452 | 0.996 | 3378 | 2.1 | 1.080 | 3455 | -0.1 | 1.137 | 3406 | 1.3 |
| 15 | 3529 | 0.996 | 3378 | 4.3 | 1.080 | 3455 | 2.1 | 1.177 | 3790 | -7.4 |
| 16 | 3606 | 0.996 | 3378 | 6.3 | 1.092 | 3577 | 0.8 | 1.190 | 3919 | -8.7 |
| 17 | 3813 | 1.021 | 3646 | 4.4 | 1.092 | 3577 | 6.2 | 1.150 | 3529 | 7.5 |
| 18 | 4023 | 1.033 | 3779 | 6.1 | 1.139 | 4121 | -2.4 | 1.203 | 4049 | -0.6 |
| 19 | 4103 | 1.058 | 4050 | 1.3 | 1.127 | 3987 | 2.8 | 1.190 | 3919 | 4.5 |
| 20 | 4278 | 1.058 | 4050 | 5.3 | 1.174 | 4533 | -6.0 | 1.243 | 4464 | -4.3 |
| 21 | 4482 | 1.082 | 4348 | 3.0 | 1.150 | 4256 | 5.0 | 1.216 | 4185 | 6.6 |
| 22 | 4675 | 1.132 | 4962 | -6.1 | 1.197 | 4829 | -3.3 | 1.269 | 4755 | -1.7 |
| 23 | 4885 | 1.107 | 4656 | 4.7 | 1.197 | 4829 | 1.2 | 1.309 | 5198 | -6.4 |
| 24 | 5370 | 1.144 | 5123 | 4.6 | 1.232 | 5281 | 1.7 | 1.349 | 5672 | -5.6 |
| 25 | 5721 | 1.194 | 5812 | -1.6 | 1.256 | 5607 | 2.0 | 1.336 | 5509 | 3.7 |
| 26 | 6094 | 1.219 | 6159 | -1.1 | 1.279 | 5943 | 2.5 | 1.362 | 5826 | 4.4 |
| 27 | 6214 | 1.231 | 6336 | -2.0 | 1.314 | 6450 | -3.8 | 1.402 | 6334 | -1.9 |
| 28 | 7173 | 1.318 | 7673 | -7.0 | 1.384 | 7530 | -5.0 | 1.481 | 7400 | -3.2 |
| 29 | 7652 | 1.330 | 7868 | -2.8 | 1.396 | 7732 | -1.0 | 1.495 | 7570 | 1.1 |
| 30 | 8042 | 1.342 | 8077 | -0.4 | 1.407 | 7911 | 1.6 | 1.508 | 7769 | 3.4 |

## V CONCLUSIONS

A simple water discharge device was presented. Theoretical results were compared with measured laboratory data. A model has been proposed to estimate the dimensionless discharge value. The following conclusions have been drawn from the present study.
1- Simple semicircular mobile flume can be used as a mobile discharge measurement device in semicircular open channels. The discharge can be estimated directly using the proposed model, which incorporates the semicircular pipe, the diameter of the vertical cylinder and the column head reading. The proposed model incorporates all the influencing parameters governing the flow. The actual measured flow rates were compared with the calculated flow rates and the proposed model \{Equations (15) through (17)\}. Results of the comparison showed that the proposed model can predict accurate discharge with a maximum error of up to $8.6 \%$.

2- Also, the discharge can be estimated directly using the proposed mathematical model \{Equations (11) and (14)\}, which incorporates the semicircular pipe, diameter of the vertical cylinder and the column head reading. Proposed model incorporates all the influencing parameters governing the flow. The actual measured flow rates were compared with the calculated flow rates and corrected by Equations (19) through (21). Results of the comparison showed that the proposed mathematical model \{Equation (14)\} predicted approximately the same accurate discharge with a maximum error up to $8.7 \%$ as compared to the measured discharge.
3- A relative critical water depth plot as ordinate against the dimensionless specific energy as abscissa Fig. (6) appeared approximately as a straight line for specific energy less than 0.5 regardless of the device diameter. The final result corresponds to an explicit equation for critical water depth once the specific energy height in the vertical pipe at contraction section is recorded.

4- Contraction ratio 0.413 is the best contraction value gave a near value for measured dimensionless discharge with least error.
5- $\quad$ Semicircular mobile flume can be used for discharge measurement in open channels with the best accuracy of $\pm 8.7 \%$ equations developed.

## List of Notation

$A \quad$ is the area of the water section;
$A_{*} \quad$ is dimensionless water section area $\left(A / D^{2}\right)$;
$A_{* c} \quad$ is dimensionless critical water section area $\left(A_{c} / D^{2}\right)$;
$C_{d}$ is the discharge coefficient;
$d \quad$ is vertical pipe diameter;
$d_{w} \quad$ is the normal depth of the point below the water surface;
$D \quad$ is semicircular open channel pipe;
$E \quad$ is specific energy;
$E_{*} \quad$ is dimensionless specific energy $(E / D)$;
$E_{*_{c}} \quad$ is dimensionless critical specific energy $\left(E_{c} / D\right)$;
$E_{* m e}$ is dimensionless measured specific energy $\left(E_{m e} / D\right)$;
Fr is Froude Number
$g \quad$ is the gravitational acceleration.
$Q \quad$ is discharge;
$Q_{\text {cal }}$ is calculated discharge;
$Q_{m e}$ is measured discharge;
$Q_{*} \quad$ is dimensionless discharge $\left(Q^{2} / g D^{5}\right)^{1 / 2}$;
$Q_{*_{c a l}}$ is dimensionless calculated discharge $\left(Q_{\text {cal }}^{2} / g D^{5}\right)^{1 / 2}$;
$Q_{* m e}$ is dimensionless measured discharge $\left(Q_{m e}^{2} / g D^{5}\right)^{1 / 2}$;
$R \quad$ is factor;
$T \quad$ is top width;
$T_{c} \quad$ is dimensionless critical top width;
$V \quad$ is the stream line velocity and
$y$ is water depth;
$Y \quad$ is dimensionless water depth $(y / D)$;
$Y_{c} \quad$ is dimensionless critical water depth;
$\theta \quad$ is the slope angle of the channel bottom,
$\alpha \quad$ is the energy coefficient due to variable velocity distribution,
$\delta \quad$ is contraction ratio $(d / D)$

## References

[1] U. S. Department of the Interior Bureau of Reclamation, Water Measurement Manual, A Water Resources Technical Publication, Revised Reprinted 2001.
[2] S. P. Simonovic, "an Expert System for the Selection of A Suitable Method for Flow Measurement in Open Channels", Journal of Hydrology, 112 (1990) 237-256, Elsevier Science Publishers B.V., Amsterdam Printed in the Netherlands.
[3] ISO, 1983. Measurement of liquid flow in open channels. ISO Standards Handbook, 16, 518 pp .
http://www.iso.org/iso/iso_catalogue/catalogue_tc/catalogue_tc_browse.htm? commid=51690
[4] ISO, 1986. Liquid flow measurement in open channels, General guidelines for the selection of methods. ISO 8363, 6 pp .
[5] A. Balloffet, "Critical flow meters", Journal of the Hydraulics Division ASCE 81(HY4), 1955, 1-31.
[6] M. H. Diskin, "Temporary flow measurement in sewers and drains". Journal of Hydraulics Division ASCE 89(HY4): 141-159; 90(HY2): 383387; 90(HY6): 241-247.
[7] W. H. Hager, "Modified Venturi channel", Journal of Irrigation and Drainage Engineering, ASCE, Vol. 111, No. 1, March 1985.
[8] W. H. Hager, 'Venturi Flumes of Minimum Space Requirements", Journal of Irrigation and Drainage Engineering, ASCE, Vol. 114, No. 2, May 1988, pp. 226-243.
[9] W. H. Hager, "Wastewater Hydraulics theory and Practice", © SpringerVerlag Berlin Heidelberg 2010.
[10] Peruginelli A. and Bonacci F., Mobile Prism for Flow Measurement in Rectangular Channel, Journal of Irrigation and Drainage Engineering, ASCE, Vol. 123, No. 3, May 1997.
[11] Z. Samani, and H. Magallanez, "Simple Flume for Flow Measurement in Open Channel", Journal of Irrigation and Drainage Engineering, ASCE, Vol. 126, No. 2, March 127-129, 2000.
[12] B. Wu, and A. Molinas, "Choked Flows through Short Contractions", Journal of Hydraulics Engineering, ASCE 127(8), 2001, pp. 657-662.
[13] B. Abdul Karim and D. Subhasish, "Measurement of the turbulent flow field at a vertical semicircular cylinder attached to the sidewall of a rectangular channel", Flow Measurement and Instrumentation 15 (2004) 87-96.
[14] A. Gole, "Flow meter for discharge measurement in irrigation channel", Flow measurement and instrumentation, Science Direct, Vol. 17, (2006).
[15] A. D. Ghare and A. M. Badar, "Experimental studies on the use of mobile cylinders for measurement of flow through the rectangular channel", ASCE Vol. 12 No. 4 December (2014).
[16] W. H. Hager, "Wastewater Hydraulics theory and Practice", © Springer- Verlag Berlin Heidelberg 1999, 2010.
[17] W. H. Hager, "Modified Trapezoidal Venturi channel", Journal of Irrigation and Drainage Engineering, ASCE, Vol. 112, No. 3, August 1986, pp. 225-241.
[18] Z. Samani, and H. Magallanez, "Measurement Water in Trapezoidal Canals", Journal of Irrigation and Drainage Engineering, ASCE, Vol. 119, No. 1, January 1993.
[19] A. M. Badar and A. D. Ghare, "Development of discharge prediction Model for trapezoidal canals using simple portable flume", International Journal of Hydraulic Engineering, (2012), No. 2, Vol. 1, pp. 37-42.
[20] Hager, W. H., Mobile Flume for Circular Channel, Journal of Irrigation and Drainage Engineering, ASCE, Vol. 114, No. 3, August 1988.
[21] Z. Samani, S Jorat and M. Yousef, "Hydraulic Characteristics of Circular Flume", Journal of Irrigation and Drainage Engineering, ASCE 117(4), 1991, pp. 558-566.
[22] A. Kohler, and W. H. Hager, "Mobile Flume for Pipe Flow", Journal of Irrigation and Drainage Engineering, ASCE, Vol. 123, No. 1, January 1997.
[23] J. Enciso, Evaluation of BMPs to Reduce NPS Pollution at the Farm Level, Arroyo Colorado Agricultural Nonpoint Source Assessment, Texas State Soil and Water Conservation Board (TSSWCB), U.S.A., Task 7 Report, May 2012.
[24] I.M.H. Rashwan, and M.I. Idress, "Evaluation efficiency for mobile flume as discharge measurement device for partially filled circular channel", Ain Shams Engineering journal, Elsiver, November 2, 2012.
[25] S. Davis and Z. Samani, "Simple Flow Measurement Devices for Open Channels", June 2016.
[26] Z. Samani, Three Simple Flumes for Flow Measurement in Open Channels, Journal of Irrigation and Drainage Engineering, ASCE, February 2017.
[27] V. T. Chow, "Open channel hydraulics, International Student ed. McGraw-Hill Kogakusha Ltd.; 1959.


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